

UNIVERSITY OF BOLTON
SCHOOL OF ENGINEERING
BENG MECHANICAL ENGINEERING
SEMESTER ONE EXAMINATION 2021/2022
ADVANCED THERMOFLUID AND CONTROL
SYSTEMS
MODULE NO: AME6015

Date: Tuesday 11th January 2022

Time: 10:00 – 12:00

INSTRUCTIONS TO CANDIDATES:

There are **SIX** questions.

Answer **FOUR** questions.

All questions carry equal marks.

Marks for parts of questions are shown in brackets.

This examination paper carries a total of 100 marks.

All working must be shown. A numerical solution to a question obtained by programming an electronic calculator will not be accepted.

CANDIDATES REQUIRE:

Formula Sheets (attached following questions).

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Question 1

a) Steam is at 22 bar and has enthalpy of 2750KJ/Kg. Find the dryness fraction, specific volume and internal energy

(12 Marks)

b) A Reversible engine operates between temperature of 400°C and 2800°C, the heat being supplied is at the rate of 300KJ/s. Determine its efficiency and power output.

(8 Marks)

c) A Steam Power Plant working on the Carnot cycle operates between 1 bar 99.6°C and 10 bar 179.92 °C. Determine the pressure, temperature and entropy of all points and draw the cycle on the P-V and T-S diagram.

(5 Marks)

Total 25 Marks

Question 2

a) The phenomenon of drag is of consideration important to engineers involved in the design of vehicles. The drag F on a fully submerged smooth sphere of diameter D depends on its velocity V , the density of fluid ρ , and the viscosity of the fluid μ . Arrange these variables into independent dimensionless numbers.

(15 Marks)

b) Gasoline at a temperature of 20°C ($\nu=4.5 \times 10^{-7} \text{ m}^2/\text{s}$) flows through a flexible pipe from a gas pump to the gas tank of a car. If 3L/s are flowing and the pipe has an inside diameter of 60mm, what is the Reynolds number? Is the flow laminar or turbulent?

(10 Marks)

Total 25 Marks

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Question 3

a) The Radiator of a steam heating system has a volume of 15L and is filled with superheated water vapour at 200Kpa and 200 degrees Celsius. At this moment both the inlet and the exit valves are closed. After a while the temperature of the steam drops to 80 degrees Celsius as a result of heat transfer to the room air. Determine the entropy change of the steam during this process.

(10 Marks)

b) i) Determine the head loss due to a flow of 100l/s of glycerine at 20°C through 100m of 20cm diameter pipe. Glycerine has a specific gravity of 1.26 and Viscosity 0.886 Ns/m².

ii) Rework the problem for water as fluid, with density = 1000Kg/m³ at 20°C and viscosity of 1.005×10⁻³ Ns/m². For water use the Moody diagram provided in the Appendix with $\epsilon=0.025\text{cm}$.

(15 Marks)

Total 25 Marks

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Question 4

- a) Derive the differential equations describing the behaviour of the spring-mass-damper system shown in **Figure Q4**. (8 Marks)
- b) Select the state variables and transfer the differential equations obtained from 4a into the state-space representation. (10 Marks)
- c) Determine the state space equations and system matrices A, B, C and D, where A, B, C, and D have their usual meaning, and the output variable are y_1 and \dot{y}_1 . (4 Marks)
- d) Evaluate the system matrices A, B, C and D for $m_1 = 2$, $m_2 = 5$, $k_1 = 10$, $k_2 = 6$ and $c_2 = 0.2$. (3 Marks)

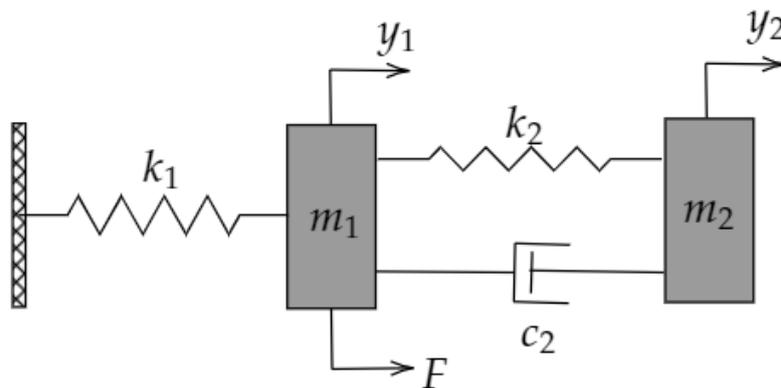


Figure Q4: Spring-mass-damper system with two masses.

Total 25 Marks

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Question 5

A PID controller is used to control an automation processing plant as shown in Figure Q5. The open loop transfer function of the plant is given by

$$G_p(s) = \frac{60}{(s + 2)(s + 5)}$$

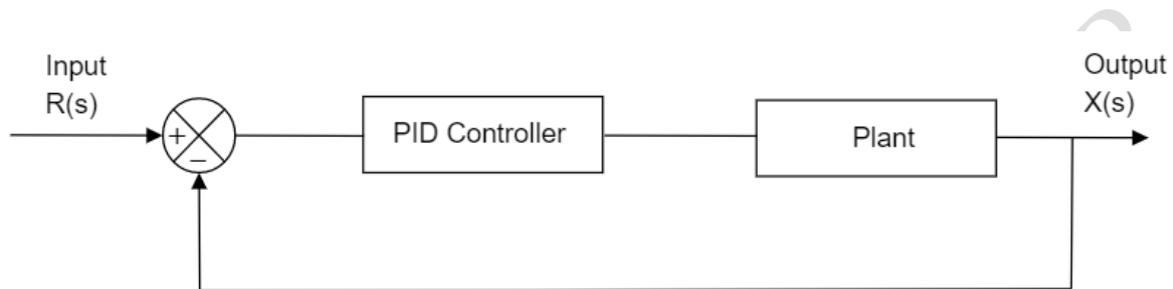


Figure Q5: Control system of the processing plant.

- (a) Evaluate the performances of closed loop plant system (natural frequency, damping ratio, Percentage Overshoot, peak time, settling time and steady-state error) to assess its performance without the PID controller.

(10 Marks)

- (b) Design a PID controller to determine the parameter K_p , K_i and K_d , and clearly identify the design procedure if the system responses for a unit step input are required as:

- The maximum overshoot is less than 8%.
- The settling time is 40% less than that of without the PID controller.
- The steady-state error is 0.

(15 Marks)

Total 25 Marks

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Question 6

The transfer function of a servo control system is given as

$$G(s) = \frac{100}{(s + 2)(s + 10)}$$

a) Draw the asymptotic Bode plot.

(15 Marks)

b) Draw the Nyquist plot using the ω values at 0, 0.5, 1, 2, 3, 5, 10 and 100.

(10 Marks)

Total 25 Marks

END OF QUESTIONS

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Formula sheet

Blocks with feedback loop

$$G(s) = \frac{Go(s)}{1 + Go(s)H(s)} \text{ (for a negative feedback)}$$

$$G(s) = \frac{Go(s)}{1 - Go(s)H(s)} \text{ (for a positive feedback)}$$

Steady-State Errors

$$e_{ss} = \lim_{s \rightarrow 0} [s \frac{1}{1 + G_o(s)} \theta_i(s)] \text{ (for the closed-loop system with a unity feedback)}$$

$$e_{ss} = \lim_{s \rightarrow 0} [s \frac{1}{1 + \frac{G_o(s)}{1 + G_o(s)[H(s) - 1]}} \theta_i(s)] \text{ (if the feedback } H(s) \neq 1)$$

$$e_{ss} = \frac{1}{1 + \lim_{z \rightarrow 1} G_o(z)} \text{ (if a digital system subjects to a unit step input)}$$

Laplace Transforms

A unit impulse function 1

A unit step function $\frac{1}{s}$

A unit ramp function $\frac{1}{s^2}$

First order Systems

$$G(s) = \frac{\theta_o}{\theta_i} = \frac{G_u(s)}{\tau s + 1}$$

$$\tau \left(\frac{d\theta_o}{dt} \right) + \theta_o = G_u \theta_i$$

$$\theta_o = G_u (1 - e^{-t/\tau}) \text{ (for a unit step input)}$$

$$\theta_o = A G_u (1 - e^{-t/\tau}) \text{ (for a step input with size A)}$$

$$\theta_o(t) = G_u \left(\frac{1}{\tau} \right) e^{-t/\tau} \text{ (for an impulse input)}$$

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Second-order systems

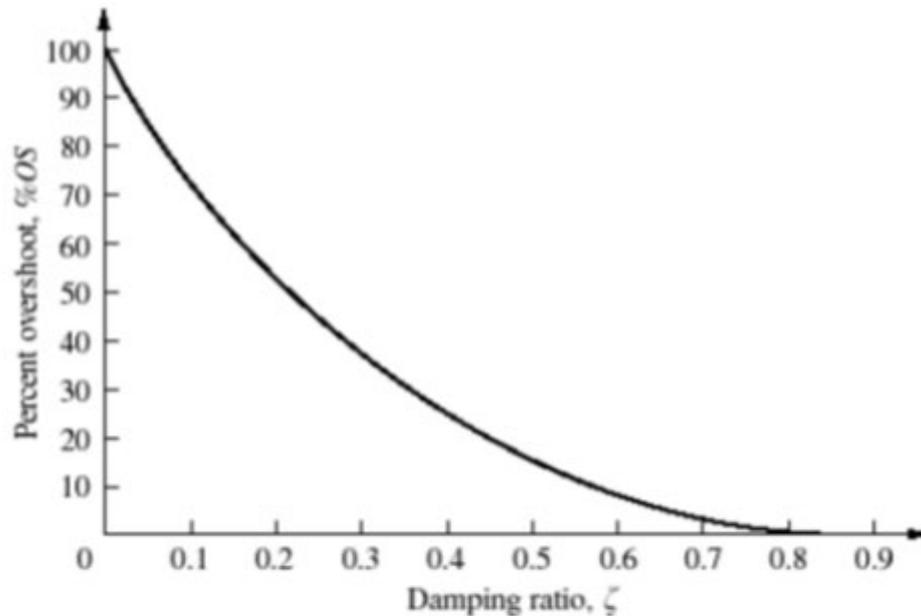
$$\frac{d^2\theta_o}{dt^2} + 2\zeta\omega_n \frac{d\theta_o}{dt} + \omega_n^2\theta_o = b_o\omega_n^2\theta_i$$

$$G(s) = \frac{\theta_o(s)}{\theta_i(s)} = \frac{b_o\omega_n^2}{s^2 + 2\zeta\omega_n s + \omega_n^2}$$

$$\omega_{dr} = 1/2\pi \quad \omega_{dp} = \pi$$

$$\text{P.O.} = \exp\left(\frac{-\zeta\pi}{\sqrt{1-\zeta^2}}\right) \times 100\%$$

$$t_s = \frac{4}{\zeta\omega_n} \quad \omega_d = \omega_n\sqrt{1-\zeta^2}$$



Controllability: $R = [B \ AB \ A^2B \ \dots \ A^{(n-1)}B]$

Observability:

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Laplace Transforms of common functions

Functions		
Unit pulse (Dirac delta distribution)	$\delta(t)$	$F(s) = 1$
Unit step function	$1(t)$	$F(s) = \frac{1}{s}$
Ramp function	$f(t) = at$	$F(s) = \frac{1}{s^2}$
Sine function	$f(t) = \sin at$	$F(s) = \frac{a}{s^2 + a^2}$
Cosine function	$f(t) = \cos at$	$F(s) = \frac{s}{s^2 + a^2}$
Exponential function	$f(t) = e^{at}$	$F(s) = \frac{1}{s - a}$
Operations		
Differentiation	$L(f'(t))$	$sF(s) - f(0)$
Integration	$L\left(\int f(t) dt\right)$	$\frac{1}{s}F(s)$
Time shift	$Lf(t - a)$	$e^{-as}F(s)$

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$$W = \frac{P_1 V_1 - P_2 V_2}{n-1} \quad W = P (v_2 - v_1)$$

$$W = PV \ln\left(\frac{V_2}{V_1}\right)$$

$$Q = C_d A \sqrt{2gh}$$

$$V_1 = C \sqrt{2g h_2 \left(\frac{\rho_{\text{gas}}}{\rho_{\text{liq}}} - 1\right)}$$

$$\sum F = \frac{\Delta M}{\Delta t} = \Delta M$$

$$F = \rho QV$$

$$Re = VL \rho / \mu$$

$$dQ = du + dw$$

$$du = cu dT$$

$$dw = pdv$$

$$pv = mRT$$

$$h = hf + xhf_g$$

$$s = sf + xsf_g$$

$$v = x Vg$$

$$Q - w = \sum mh$$

$$F = \frac{2\pi L \mu}{L_s \left(\frac{R_2}{R_3}\right)}$$

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$$S_g = C_{p,c} L_n \frac{T}{273} + \frac{h_{fg}}{T_f}$$

$$S = C_{p,c} L_n \frac{T_f}{273} + \frac{h_{fg}}{T_f} + C_{p,v} L_n \frac{T}{T_f}$$

$$S_2 - S_1 = MC_p L_n \frac{T_2}{T_1} - MRL_n \frac{P_2}{P_1}$$

$$F_D = \frac{1}{2} CD \rho u^2 s$$

$$F_L = \frac{1}{2} C_L \rho u^2 s$$

$$S_f = \frac{d}{ds} (P + \rho g Z)$$

$$Q = \frac{\pi D^4 \Delta p}{128 \mu L}$$

$$h_f = \frac{64}{R} \left(\frac{L}{D} \right) \left(\frac{v^2}{2g} \right)$$

$$h_f = \frac{4fL v^2}{d 2g}$$

$$f = \frac{16}{Re}$$

$$h_m = \frac{K v^2}{2g}$$

$$h_m = \frac{k(V_1 - V_2)^2}{2g}$$

$$\zeta = \left(1 - \frac{T_L}{T_H} \right)$$

$$S_{gen} = (S_2 - S_1) + \frac{Q}{T}$$

$$W = (U_1 - U_2) - T_o(S_1 - S_2) - T_o S_{gen}$$

$$W_s = W - P_o(V_2 - V_1)$$

$$W_{rev} = (U_1 - U_2) - T_o(S_1 - S_2) + P_o(V_1 - V_2)$$

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$$\Phi = (U - U_0) - T(S - S_0) + P_0(V - V_0)$$

$$I = T_0 S_{gen}$$

$$V = r\omega$$

$$\lambda = \mu \frac{V}{t}$$

$$F = \frac{2\pi L \mu u}{L_n \left(\frac{R_2}{R_1} \right)}$$

$$T = \frac{\pi^2 \mu N}{60t} (R_1^4 - R_2^4)$$

$$p = \frac{\rho g Q H}{1000}$$

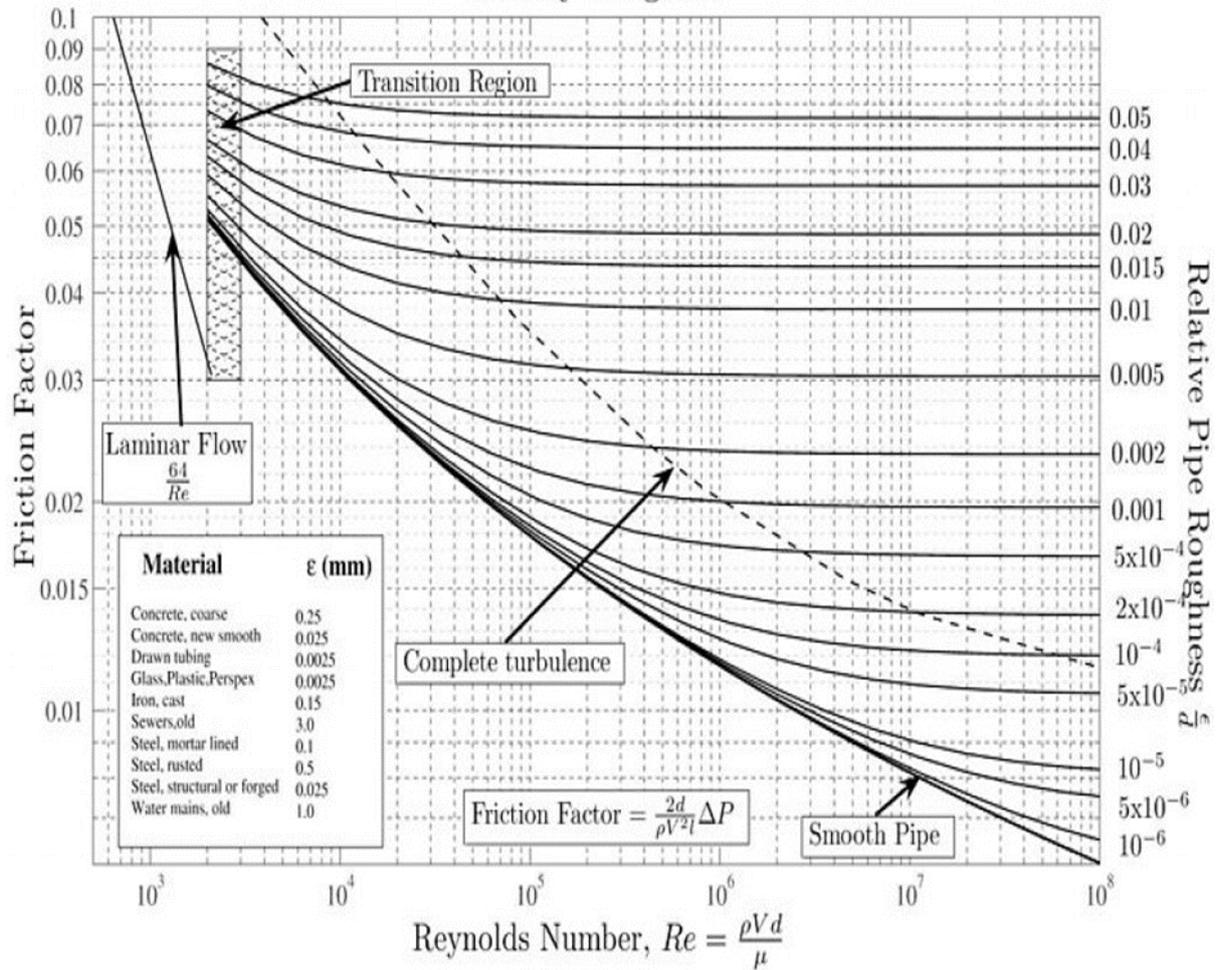
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Moody Diagram



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DIMENSIONS FOR CERTAIN PHYSICAL QUANTITIES

Quantity	Symbol	Dimensions	Quantity	Symbol	Dimensions
Mass	m	M	Mass /Unit Area	m/A^2	ML^{-2}
Length	l	L	Mass moment	ml	ML
Time	t	T	Moment of Inertia	I	ML^2
Temperature	T	θ	-	-	-
Velocity	u	LT^{-1}	Pressure /Stress	p/σ	$ML^{-1}T^{-2}$
Acceleration	a	LT^{-2}	Strain	τ	$M^0L^0T^0$
Momentum/Impulse	mv	MLT^{-1}	Elastic Modulus	E	$ML^{-1}T^{-2}$
Force	F	MLT^{-2}	Flexural Rigidity	EI	ML^3T^{-2}
Energy - Work	W	ML^2T^{-2}	Shear Modulus	G	$ML^{-1}T^{-2}$
Power	P	ML^2T^{-3}	Torsional rigidity	GJ	ML^3T^{-2}
Moment of Force	M	ML^2T^{-2}	Stiffness	k	MT^{-2}
Angular momentum	-	ML^2T^{-1}	Angular stiffness	T/η	ML^2T^{-2}
Angle	η	$M^0L^0T^0$	Flexibility	$1/k$	$M^{-1}T^2$
Angular Velocity	ω	T^{-1}	Vorticity	-	T^{-1}
Angular acceleration	α	T^{-2}	Circulation	-	L^2T^{-1}
Area	A	L^2	Viscosity	μ	$ML^{-1}T^{-1}$
Volume	V	L^3	Kinematic Viscosity	τ	L^2T^{-1}
First Moment of Area	Ar	L^3	Diffusivity	-	L^2T^{-1}
Second Moment of Area	I	L^4	Friction coefficient	f/μ	$M^0L^0T^0$
Density	ρ	ML^{-3}	Restitution coefficient		$M^0L^0T^0$
Specific heat-Constant Pressure	C_p	$L^2T^{-2}\theta^{-1}$	Specific heat-Constant volume	C_v	$L^2T^{-2}\theta^{-1}$

Note: a is identified as the local sonic velocity, with dimensions $L.T^{-1}$

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